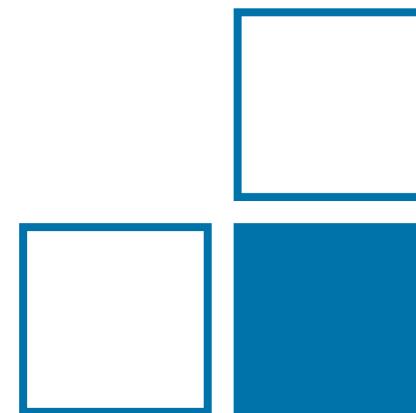


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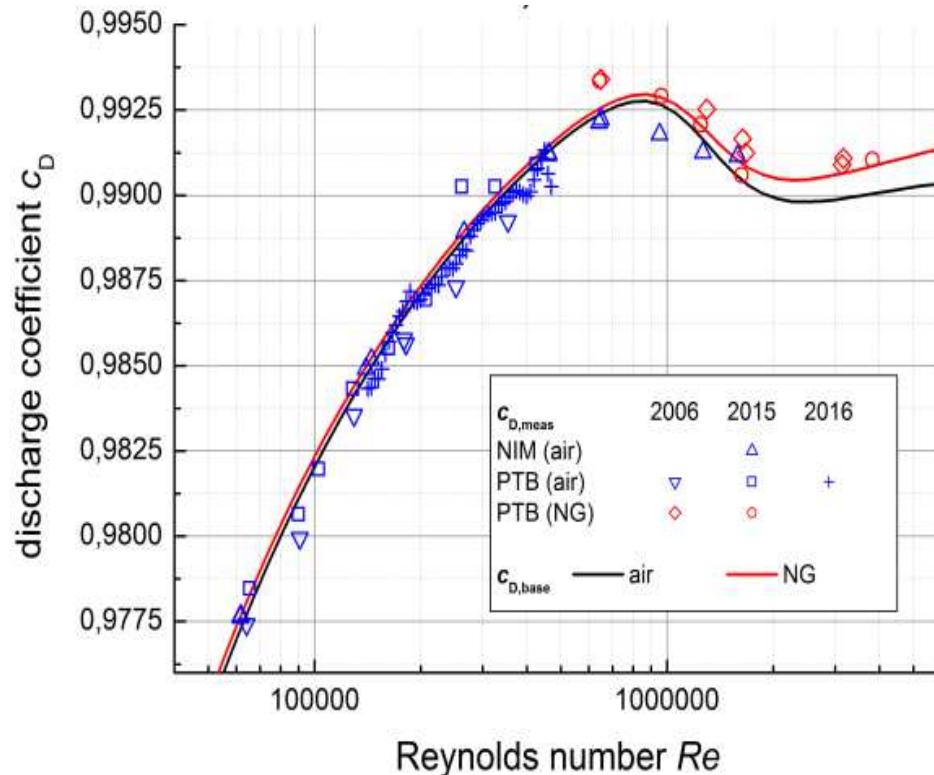
# Discharge coefficients of CFVN predicted for high Reynolds numbers based on Low-Re-calibration

Dr. Bodo Mickan  
Department High Pressure Gas  
PTB Braunschweig



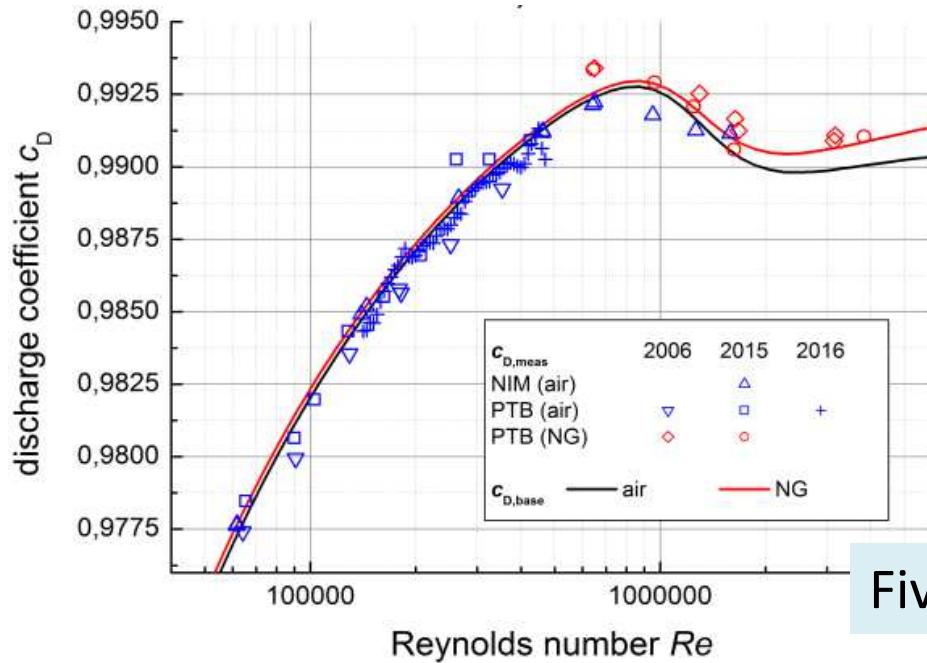
# Motivation

## Extended data analysis of bilateral comparisons with air and natural gas up to 5 MPa *FLOMEKO 2016*



- Successful introduction of a model  $c_D = f(Re)$  across laminar and turbulent
- Using only a few parameters
- Can we enhance this approach to extrapolate from LP to HP?

# 2016: Description of $c_D = f(Re)$ across transition



$$c_{D,lm} = a - b_{lm} \cdot Re^{-0.5}$$

$$c_{D,turb} = a - b_{turb} \cdot Re^{-0.139}$$

$$c_D = s_{lm} \cdot c_{D,lm} + s_{turb} \cdot c_{D,turb}$$

$$s_{lm} = 0.5 \left\{ 1 - \tanh \left[ k_u \log \left( \frac{Re}{Re_{tr}} \right) \right] \right\}$$

$$s_{turb} = 1 - s_{lm}$$

Five parameters:  $a, b_{lm}, b_{turb}, k_u, Re_{tr}$

- Fixed relation between  $b_{lm}$  and  $b_{turb}$   $b_{turb} = 0.003654 \cdot b_{lm}^{1.736}$
  - Assuming  $k_u$  as a fixed global, common parameter for all nozzles.
- ⇒ **Reduction to 3 parameter/nozzle:  $a; b_{lm}; Re_{tr}$**

**Can we reduce further down to only one parameter?**

# Further Parameter Reduction



$$c_D = a - b_{lam}/Re^{0.5}$$

Kliegel 1969

$$a = 1 - a_2 + a_3 - a_4$$

$$a_2 = \frac{\kappa + 1}{96(2R_{C,\text{throat}} + 1)^2}$$

$$a_3 = \frac{(\kappa + 1)(8\kappa - 27)}{2304(2R_{C,\text{throat}} + 1)^3}$$

$$a_4 = \frac{(\kappa + 1)(754\kappa^2 - 757\kappa + 3633)}{276480(2R_{C,\text{throat}} + 1)^4}$$

Note on  $Re_{tr}$ : also fixed on empirical base to  $Re_{tr} = 1.25 \cdot 10^6$

Geropp 1971+87

$$b_{lam} = G \cdot R_{C,\text{throat}}^{0.25}$$

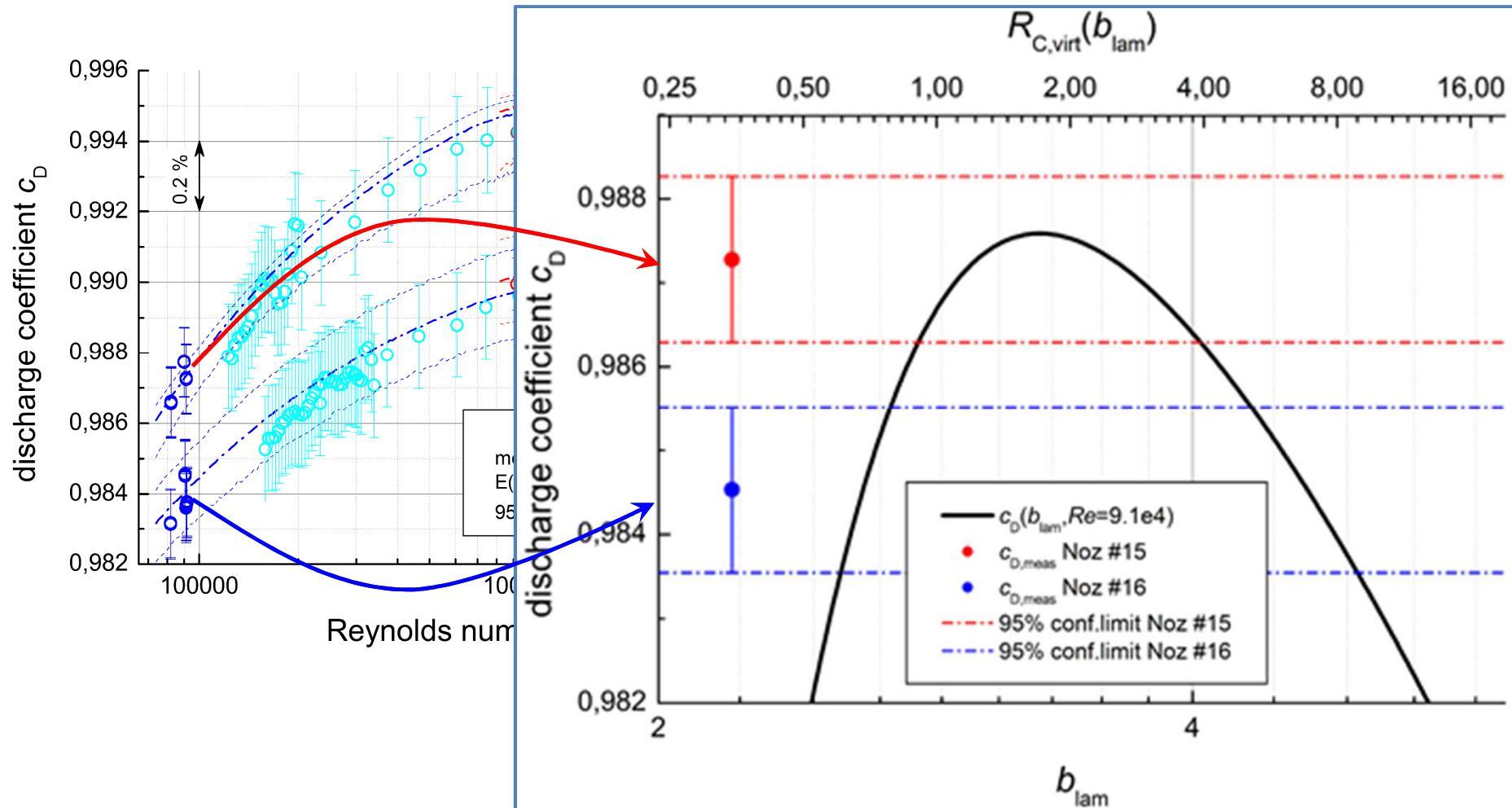
- Common parameter  $R_{C,\text{throat}}$
- real curvature radius determining these parameters probably differs from  $R_{C,\text{throat}}$
- We assume that for both the same (virtual) curvature Radius  $R_{C,\text{virt}}$  applies

$$R_{C,\text{virt}} = \left( \frac{b_{lam}}{G} \right)^4$$

$$b_{lam} \xrightarrow{(7)} R_{C,\text{virt}} \xrightarrow{(5)} a$$

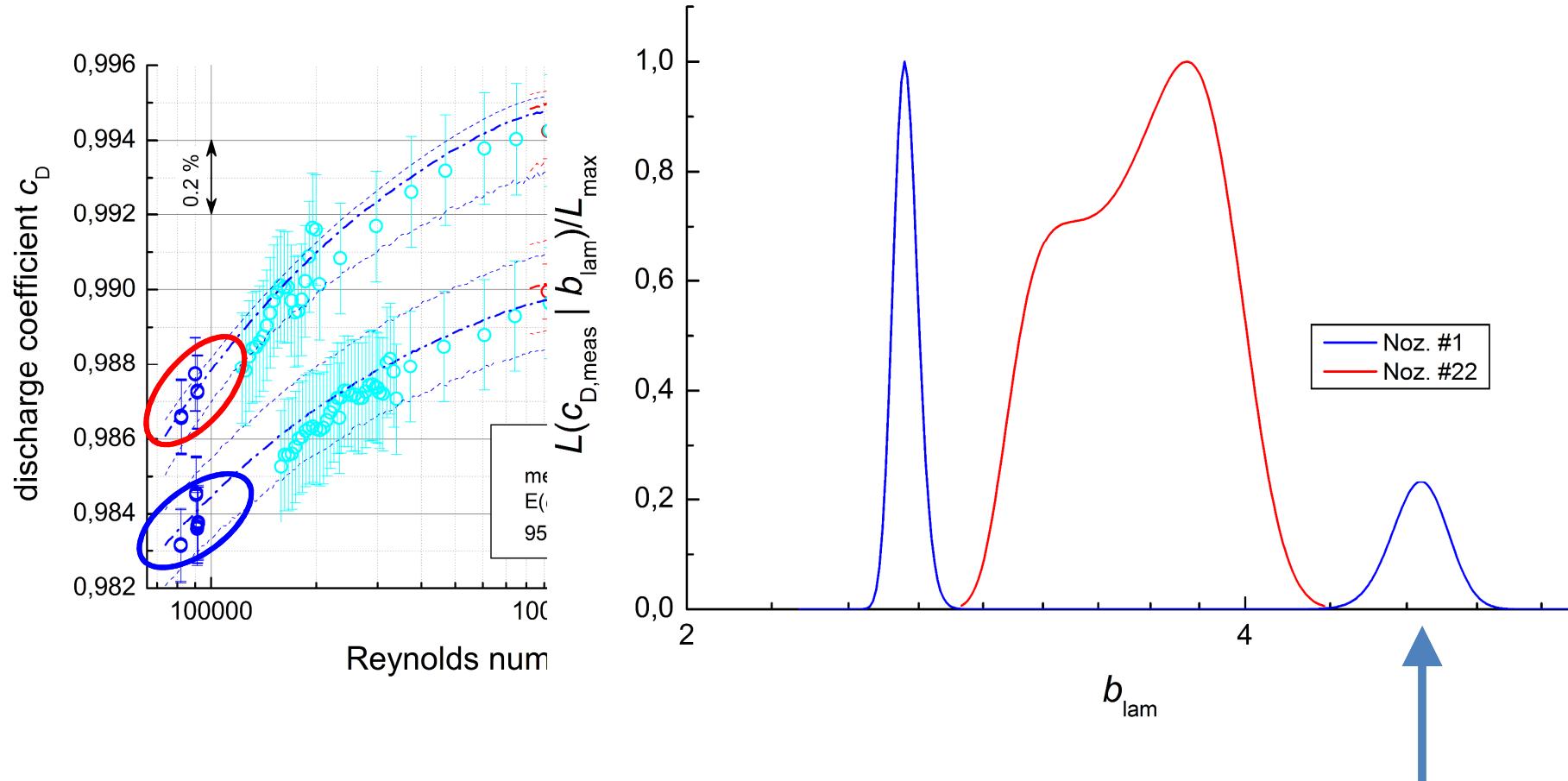
$$b_{turb} = 0.003654 b_{lam}^{1.736}$$

# $c_D$ as a function of $b_{\text{lam}}$ at a specific $Re$ -number



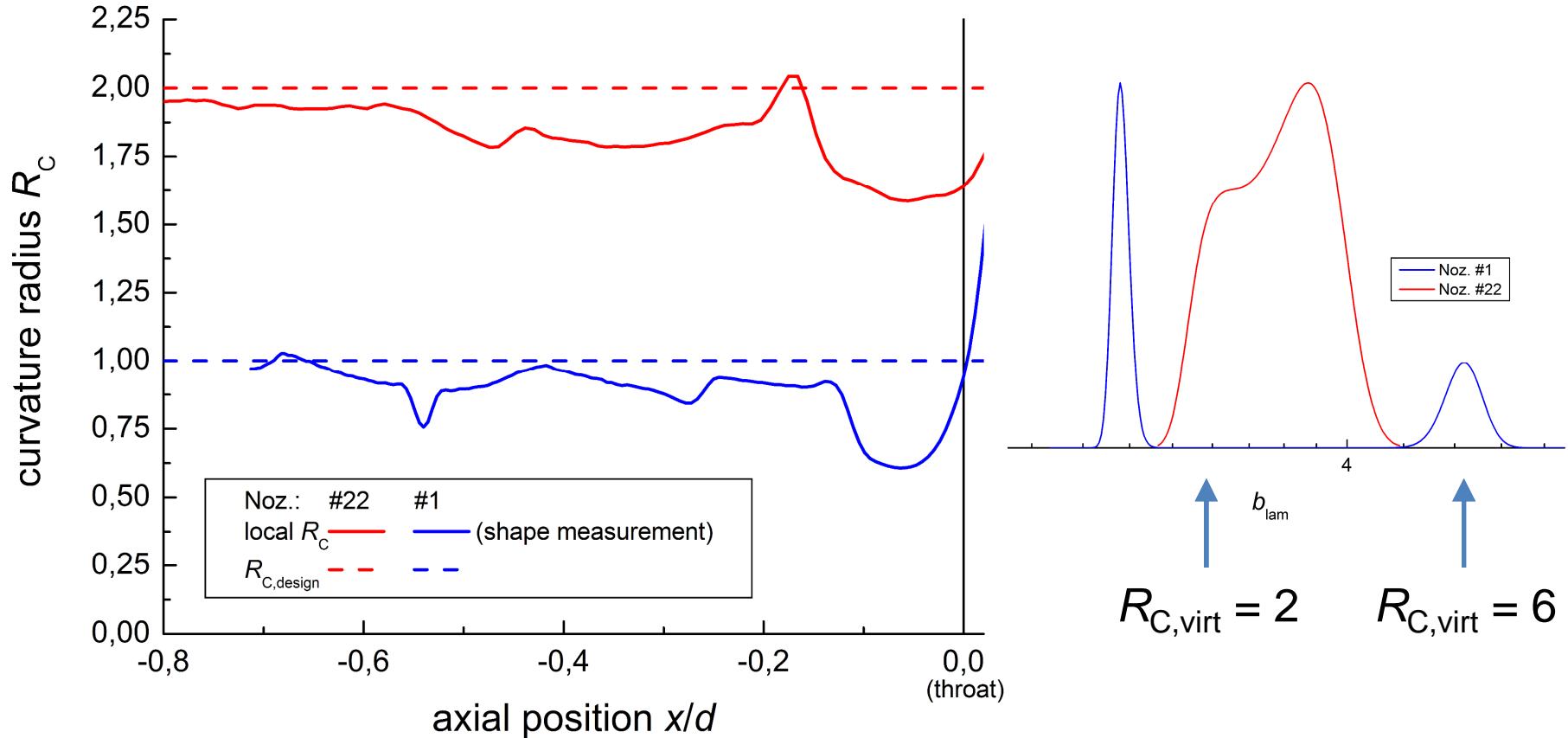
For each measured  $c_D$  we can determine the Likelihood  $L(c_{D,\text{meas}}|b_{\text{lam}})$

# Likelihood for parameter determination



Secondary peak is „disturbing“  
=> we needed further information to enhance the outcome

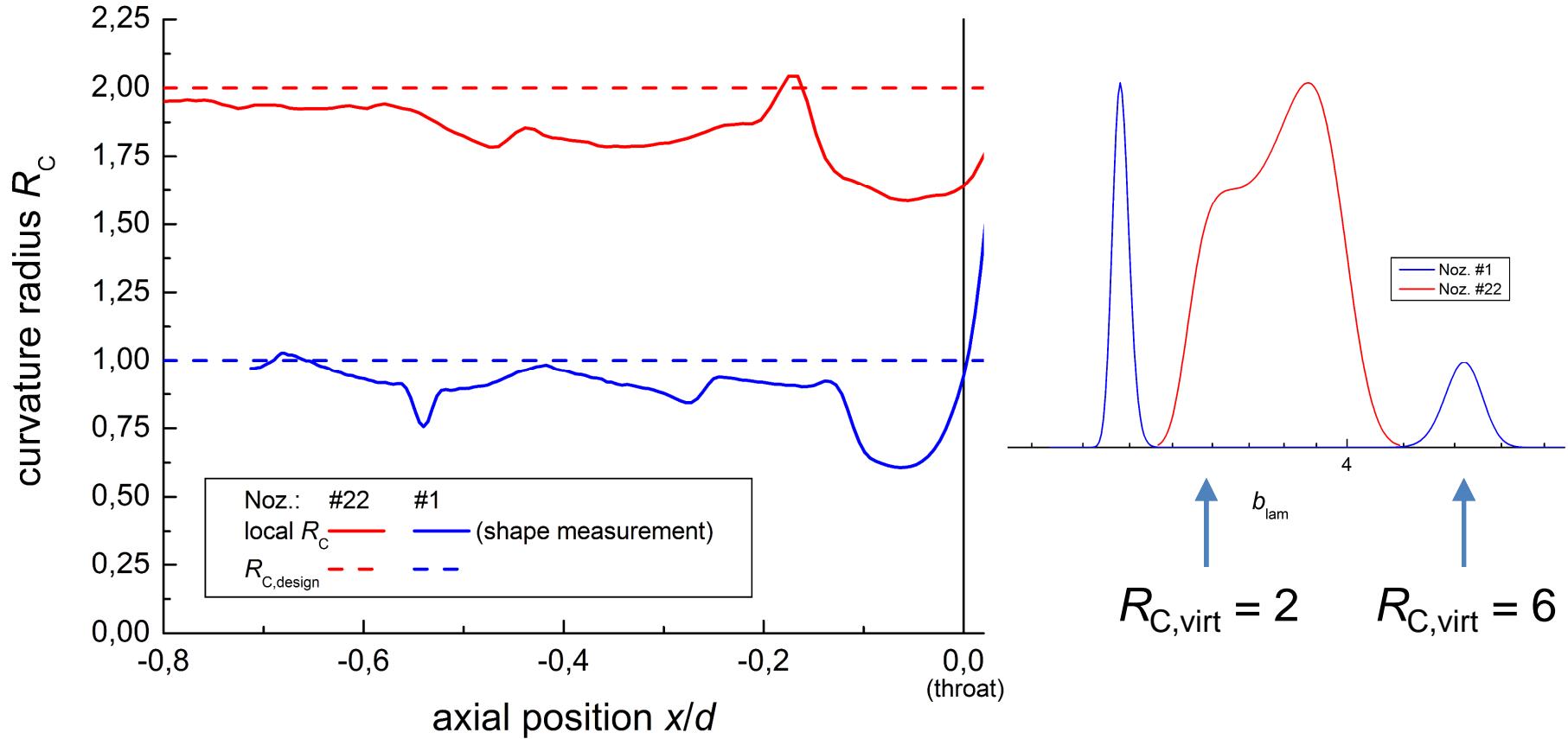
# Likelihood for parameter determination



Based on the shape information, it was reasonable to exclude unrealistic parts. The mathematical way to do this is the Bayesian approach:

$$p(b_{lam} | c_{D,meas}) \sim L(c_{D,meas} | b_{lam}) \cdot p_{prior}(b_{lam})$$

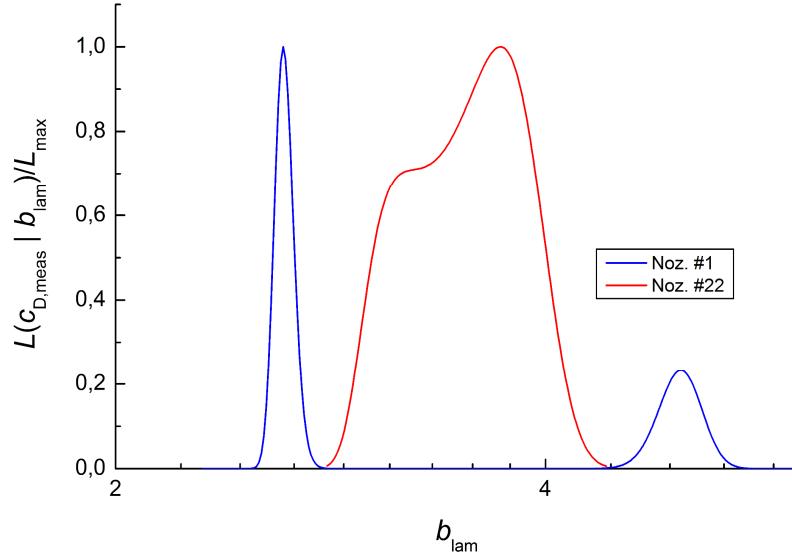
# Likelihood for parameter determination



$p_{prior} = \text{const}$  for  $0 \leq R_{C,virt} \leq 2 \cdot R_{C,design}$   
 Zero otherwise

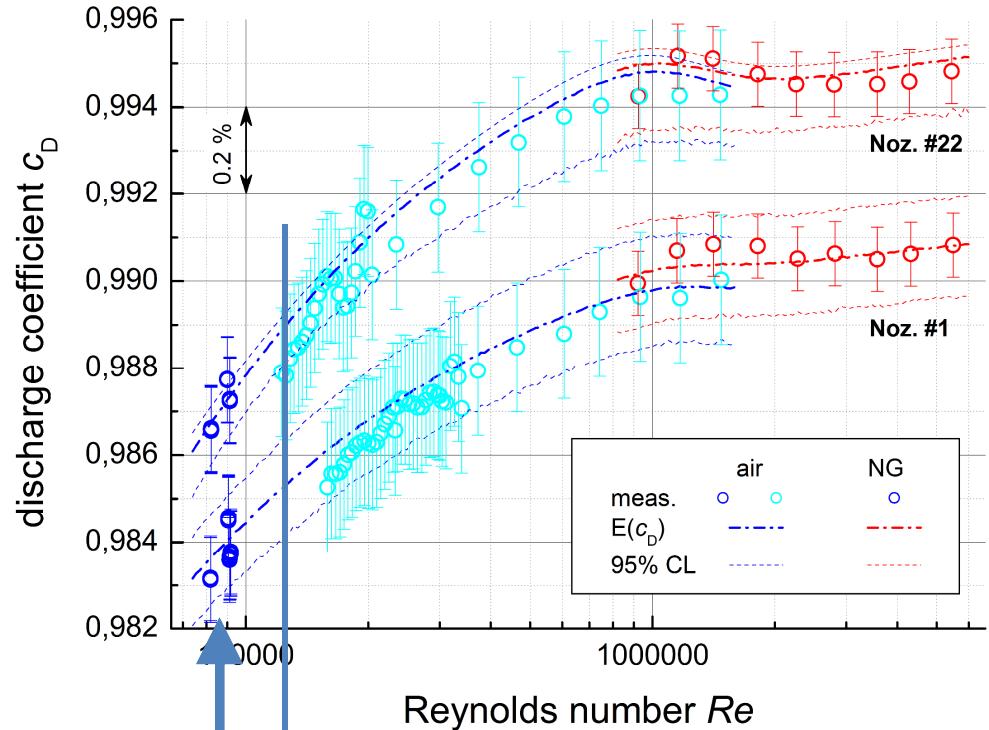
$$p(b_{lam} | c_{D,meas}) \sim L(c_{D,meas} | b_{lam}) \cdot p_{prior}(b_{lam})$$

# Likelihood for parameter determination



$$p(b_{\text{lam}} | c_{D,\text{meas}})$$

$$E(c_{D,\text{pred}})$$



Used for  
determination

Used for evaluation

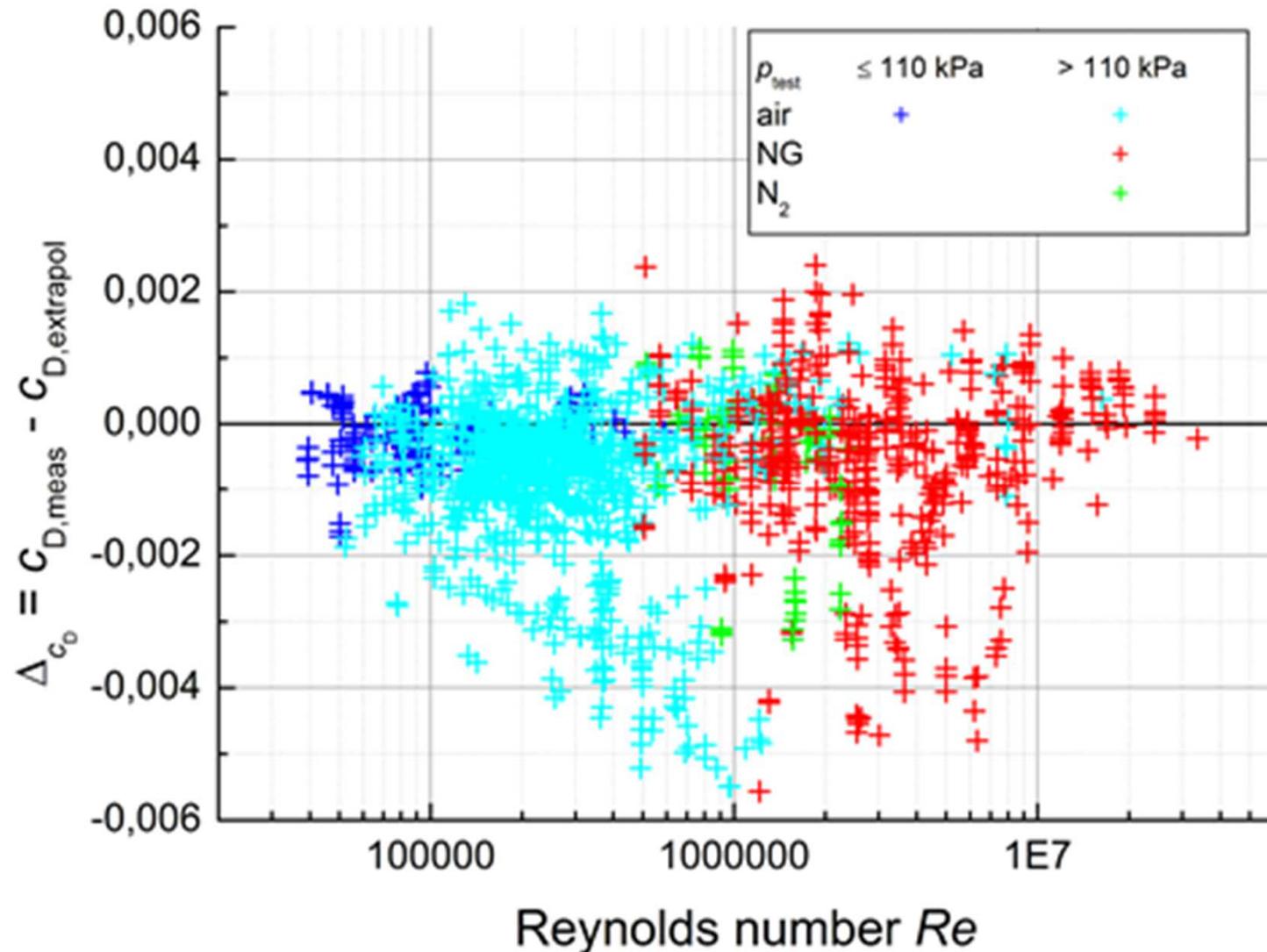
# Data Base

Noz. Nr.	$d_{throat}$ in mm	$R_{C,design}$	$Re_0$ (100 kPa, air)	for $Re/Re_0 \geq 8; k = 2$	
				$U_{Q,min,rel}$	$U_{Q,max,rel}$
1	7,098	1	9,20E4	0,07%	0,15%
2	10,780	1	1,40E5	0,16%	0,16%
3	15,250	1	1,98E5	0,16%	0,16%
4	21,320	1	2,76E5	0,16%	0,16%
5	26,950	1	3,49E5	0,16%	0,16%
6	34,280	1	4,45E5	0,16%	0,16%
7	46,560	1	6,04E5	0,16%	0,16%
8	3,808	2	4,94E4	0,07%	0,15%
9	3,893	2	5,05E4	0,15%	0,15%
10	3,897	2	5,05E4	0,19%	0,24%
11	3,903	2	5,06E4	0,15%	0,15%
12	4,331	2	5,62E4	0,19%	0,20%
13	4,344	2	5,63E4	0,19%	0,22%
14	4,938	2	6,40E4	0,12%	0,12%
15	4,945	2	6,41E4	0,08%	0,14%

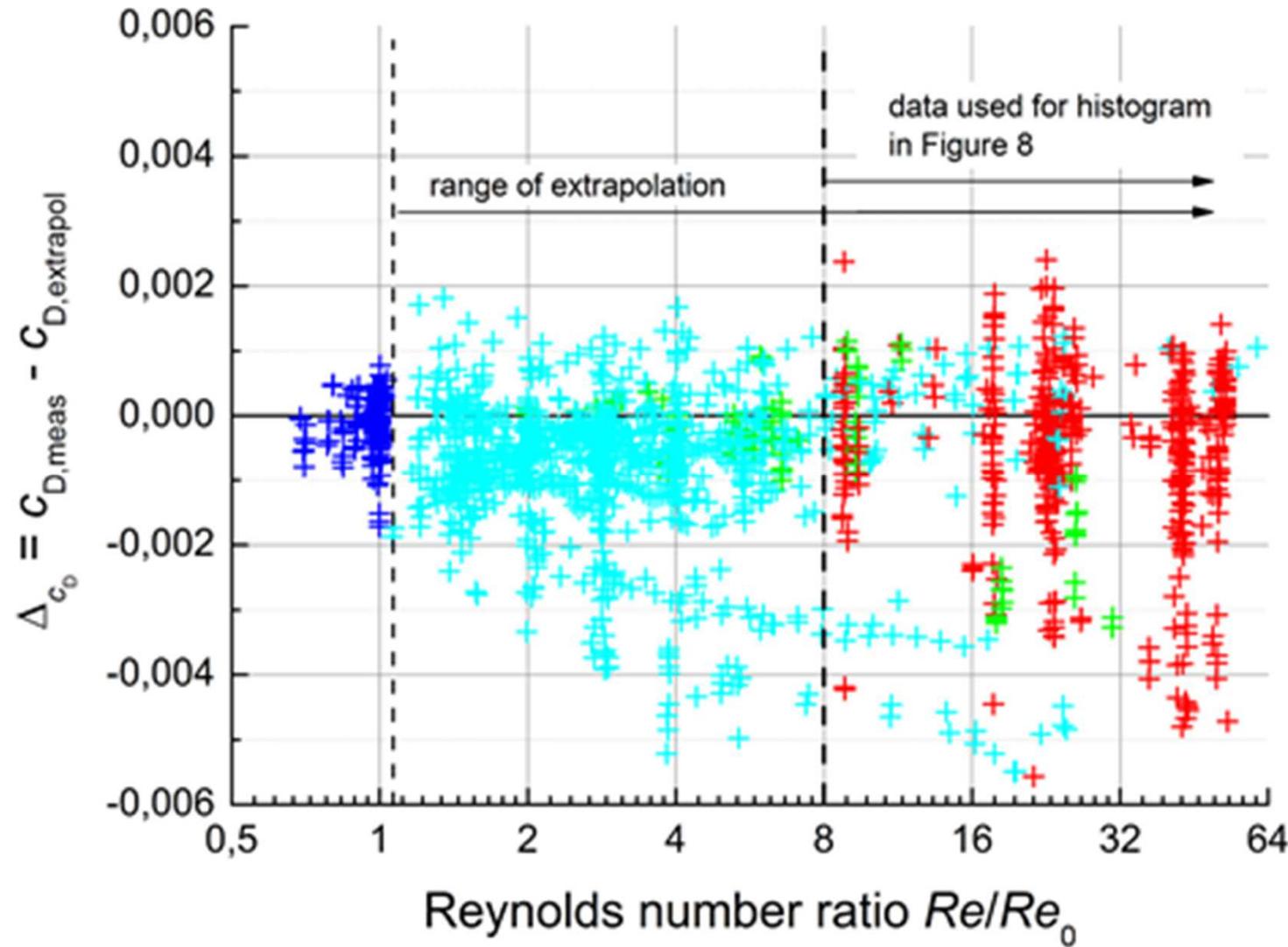
16	5,486	2	7,11E4	0,19%	0,25%
17	5,492	2	7,12E4	0,18%	0,23%
18	6,142	2	7,96E4	0,08%	0,12%
19	6,657	2	8,63E4	0,15%	0,15%
20	6,987	2	9,06E4	0,17%	0,19%
21	6,988	2	9,06E4	0,08%	0,14%
22	7,027	2	9,11E4	0,07%	0,15%
23	7,453	2	9,66E4	0,07%	0,15%
24	7,768	2	1,01E5	0,08%	0,12%
25	9,911	2	1,29E5	0,12%	0,12%
26	11,258	2	1,46E5	0,15%	0,15%
27	12,293	2	1,59E5	0,16%	0,18%
28	15,478	2	2,01E5	0,10%	0,12%
29	19,376	2	2,51E5	0,10%	0,12%
30	24,551	2	3,18E5	0,10%	0,12%
31	31,253	2	4,05E5	0,12%	0,12%
32	25,400	2,5	3,29E5	0,18%	0,19%
33	10,000	cylindr.	1,30E5	0,07%	0,13%

- 7 nozzles with  $R_{C,design} = 1$   
 24 with  $R_{C,design} = 2$   
 1 with  $R_{C,design} = 2.5$   
 1 cylindrical nozzle
- Diameter from 3.8 to 46.6 mm

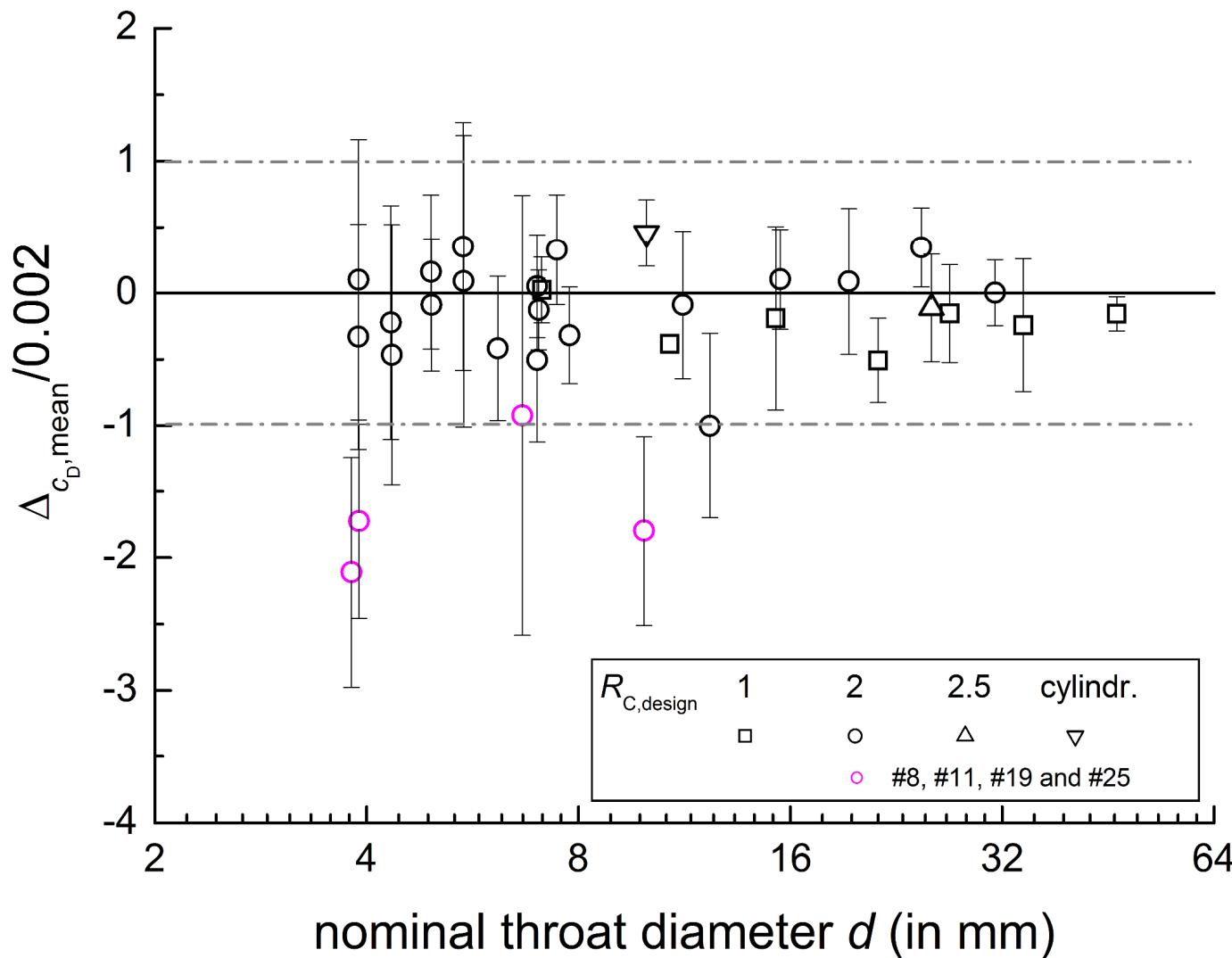
## Evaluation: $\Delta C_D = C_{D,\text{meas}} - C_{D,\text{extrapol}}$



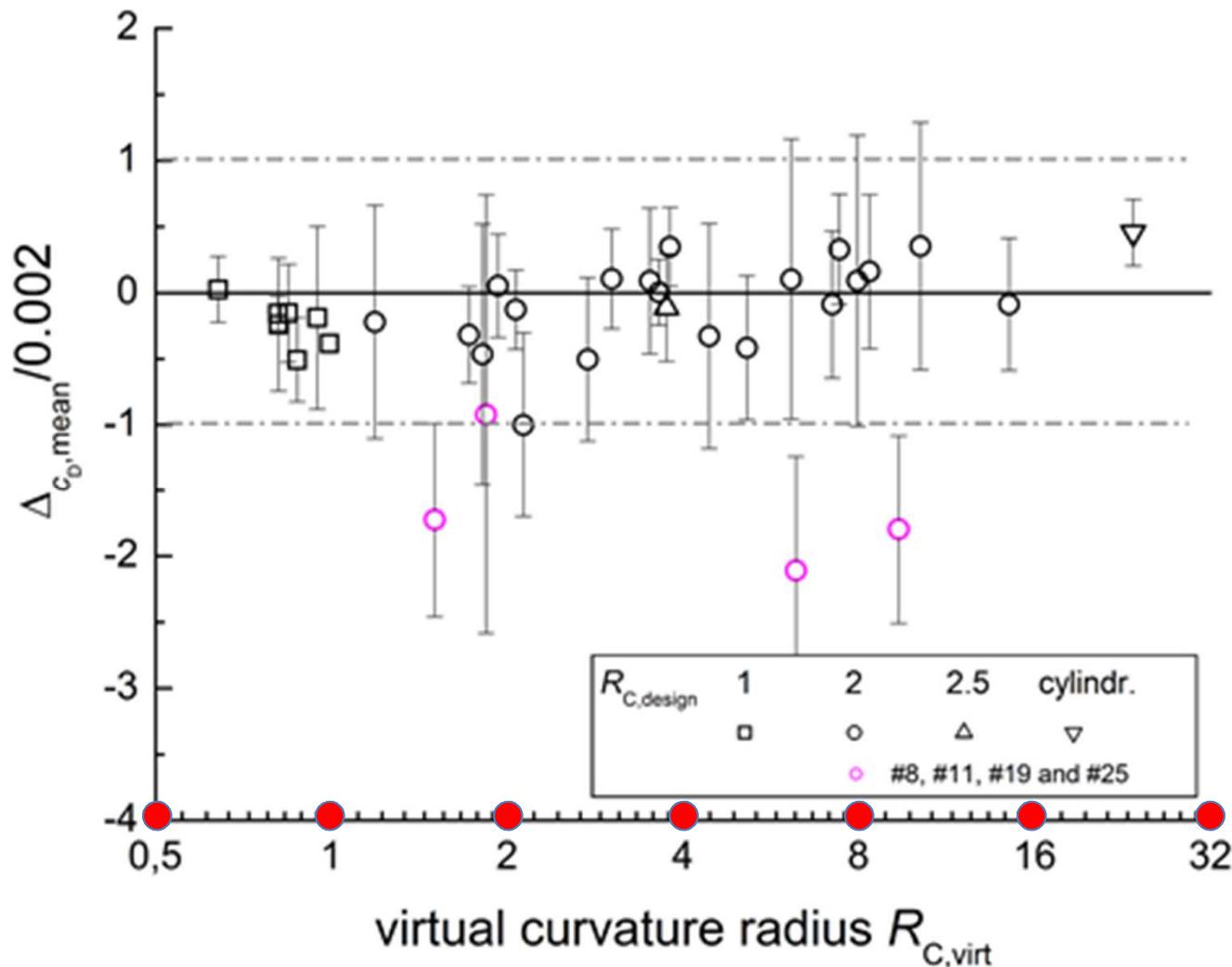
## Evaluation: $\Delta C_D = C_{D,\text{meas}} - C_{D,\text{extrapol}}$



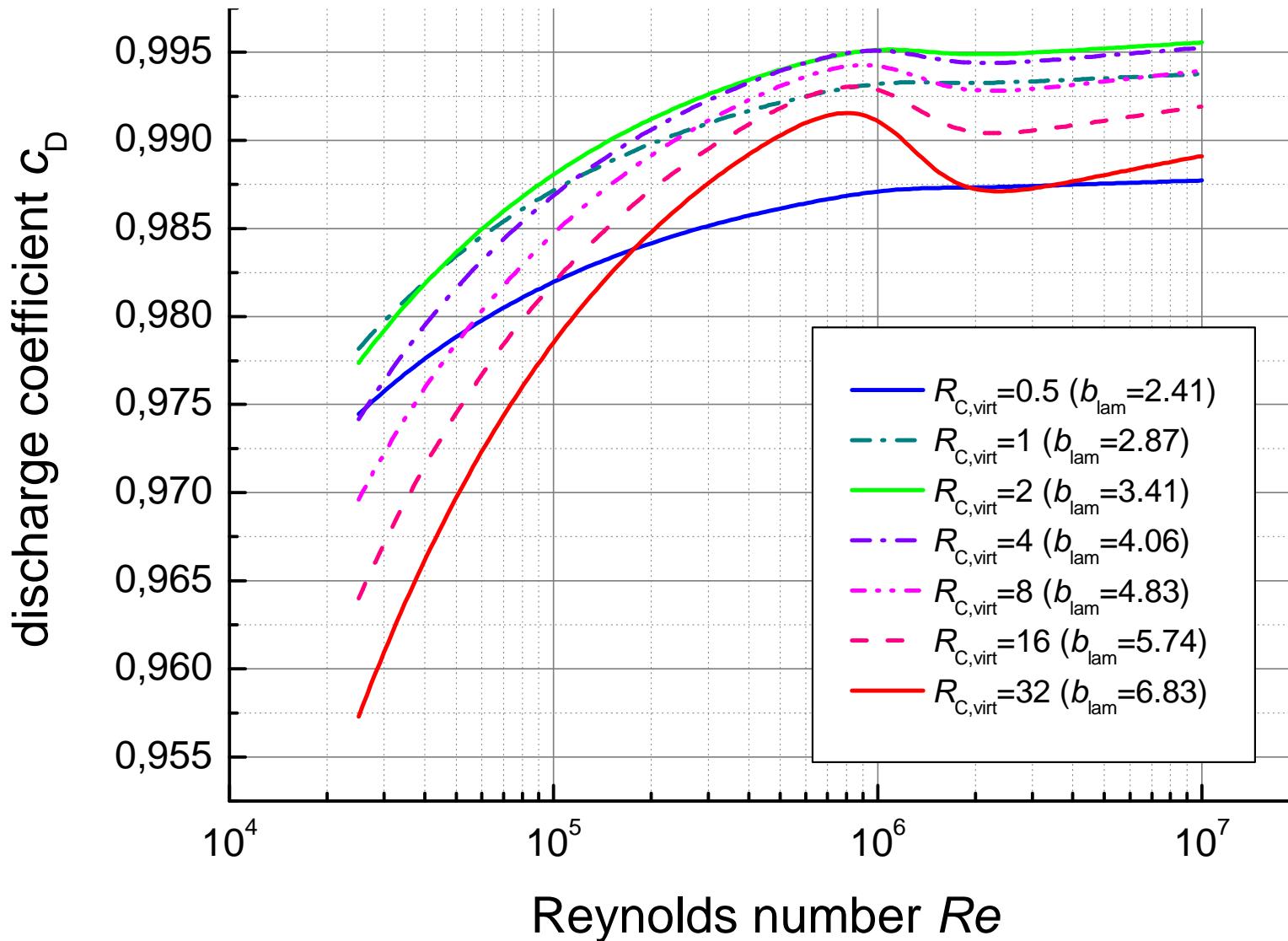
# Evaluation: $\Delta c_{D,\text{mean}}$



## Evaluation: $\Delta c_{D,\text{mean}}$



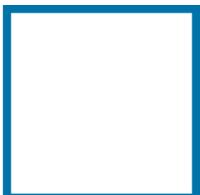
# Range of $c_D$ -values covered



# Summary and Outlook



- $c_D$ -model with only one free parameter works reliable for 29 of 33 very different nozzles with  $R_{C,\text{design}}$  from 1 to cylindrical.
- Extrapolation by factor of 60 in Reynolds up to  $Re = 3 \cdot 10^7$  is confirmed.
- The  $R_{C,\text{virt}}$  (and with this the  $c_D$  vs.  $Re$ ) differs sometimes dramatically from the design value.
- Model is restricted to hydraulic smooth surfaces.
- Approach will be extended into two directions:
  - usage of LP(Air)-calibration in wider a  $Re$ -range (e.g. 1:8)  
=> diameter can also be derived from flow measurements.
  - Bayesian approach will be refined to make better use of prior i.e. information out of dimensional measurement (diameter, shape).
- We can link our HP-traceability with the LP-traceability (see paper 1075, session S16.1, „Combining three independent traceabilities...“)



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